

8.4) HEAT ENGINE-REFRIGERATOR CASCADE

Taking the last question first, the answer to it is clearly: No. The cascade is simply another more complicated heat engine in its own right, which is subject to the Carnot limit just as the individual heat engine and refrigerator are.

The heat engine operates between the temperatures  $\tau_h$  and  $\tau_r$ . It is instructive to go beyond the problem statement and to include irreversibility. In this case, from (9) and (10), with the substitution  $\ell \rightarrow r$ ,

$$Q_r \geq (\tau_r/\tau_h)Q_h \quad , \quad (S1)$$

$$W_e = Q_h - Q_r \leq (1-\tau_r/\tau_h)Q_h \quad , \quad (S2)$$

where the equals sign holds in the reversible limit.

For the refrigerator,  $\tau_\ell$  is actually the upper temperature and  $\tau_r$  the lower temperature. If we substitute first  $\ell \rightarrow r$ , then  $h \rightarrow \ell$  in (15) and (16) we obtain

$$Q_\ell \geq (\tau_\ell/\tau_r)Q_r,$$

$$W_r = Q_\ell - Q_r \geq (\tau_\ell/\tau_r - 1)Q_r \geq (\tau_\ell/\tau_h - \tau_r/\tau_h)Q_h, \quad (S3)$$

where in the last inequality we utilized (S1). The work generated by the cascade is, with (S2) and (S3),

$$W = W_e - W_r \leq (1-\tau_r/\tau_h)Q_h - (\tau_\ell/\tau_h - \tau_r/\tau_h)Q_h = (1-\tau_\ell/\tau_h)Q_h \quad ,$$

which is the expected overall Carnot relation equivalent to (11) for the cascade.

### 8.6) ROOM AIR CONDITIONER

(a) We have  $dQ_\ell/dt = A \times (T_h - T_\ell)$ . From this and (12):

$$P = dW/dt = [(T_h - T_\ell)/T_\ell] dQ_\ell/dt = A \times (T_h - T_\ell)^2 / T_\ell \quad (S1)$$

This may be re-arranged into a quadratic equation for  $T_\ell$ :

$$T_\ell^2 - (2T_h + P/A)T_\ell + T_h^2 = 0 \quad .$$

Its relevant solution ( $T_\ell < T_h$ ) is

$$T_\ell = (T_h + P/2A) - [(T_h + P/2A)^2 - T_h^2]^{1/2} \quad .$$

(b) From (S1):

$$A = PT_\ell / (T_h - T_\ell)^2 = 2 \text{ kW} \times 290 \text{ K} / (20 \text{ K})^2 = 1.45 \text{ kW K}^{-1} \quad .$$

### 8.8) GEOHERMAL ENERGY

The work  $dW$  extractable from the heat  $dQ_h$  by a Carnot engine is, from (10),

$$dW = [(T_h - T_\ell)/T_h] dQ_h = -MC(1 - T_\ell/T_h) dT_h \quad ,$$

where  $T_h$  is the temperature at which  $dQ_h$  is removed from the rock. The total work extractable follows by integration over  $T_h$ :

$$W = - MC \int_{T_i}^{T_f} (1 - T_\ell / T_h) dT_h = - MC [T_f - T_i - T_\ell \log(T_f / T_i)] .$$

Numerically,  $MC = 10^{17} \text{ J K}^{-1}$ . The value of the brackets is -249 K. With these numbers:

$$W = 10^{17} \text{ J K}^{-1} \times 249 \text{ K} / (3.6 \times 10^6 \text{ J/kWh}) = 6.92 \times 10^{12} \text{ kWh} .$$

### 8.9) COOLING OF NON-METALLIC SOLID TO $T = 0$ .

Let  $dQ_\ell = -CdT_\ell = -aT_\ell^3 dT_\ell$  be the heat removed from the solid in lowering its temperature from  $T_\ell$  to  $T_\ell + dT_\ell$  (we assume  $dT_\ell < 0$ ). The reversible work to do so is, from (12):

$$dW = [(T_h - T_\ell) / T_\ell] dQ_\ell = - a [T_h T_\ell^2 - T_\ell^3] dT_\ell .$$

The total work required to cool the solid from  $T_\ell = T_h$  to  $T_\ell = 0$  follows by integration

$$\begin{aligned} W &= - a \int_{T_h}^0 [T_h T_\ell^2 - T_\ell^3] dT_\ell \\ &= a \left[ \frac{1}{3} T_h T_\ell^3 - \frac{1}{4} T_\ell^4 \right]_0^{T_h} = \frac{1}{12} a T_h^4 . \end{aligned}$$

### 8.10) IRREVERSIBLE EXPANSION OF A FERMI GAS

The average energy per particle remains unchanged. Initially, from (7.10) and (7.7):

$$\langle \varepsilon \rangle = 3\varepsilon_F/5 = (3\hbar^2/10M)(3\pi^2 N/V_i)^{2/3} .$$

After expansion to a concentration  $n \ll 2n_Q$  the gas behaves like an ideal gas, with  $\langle \varepsilon \rangle = 3\tau/2$ . Equating the two values:

$$\tau = 2\varepsilon_F/5 = (2\hbar^2/10M)(3\pi^2 N/V)^{2/3} . \quad (S1)$$

The condition  $n \ll 2n_Q$  can be written, with (3.63):

$$N/V_f \ll 2n_Q = 2(M\tau/2\pi\hbar^2)^{3/2} .$$

Inserting  $\tau$  from (S1):

$$N/V_f \ll (3/5)(\pi/10)^{1/2}(N/V_i) \text{ or } V_f/V_i \gg (5/3)(10/\pi)^{1/2} \cong 3 .$$

Thus any expansion by a factor large compared to 3 will do.

(a) 7860 K. (b)  $9.22 \times 10^5$  K.